

Ceramic Catalyst for the Selective Decomposition of N₂O and Method for
Making Same

Reference to Related Application

5 This is a divisional application of application Serial No. 09/786,879,
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Background of the Invention

 The invention relates to a ceramic catalyst for the selective
decomposition of N₂O (laughing gas) in a mixture of nitrous gases to N₂ and O₂
and method for making the same.

10 N₂O (laughing gas) is released in greatly differing processes as, for
example, in fluidized-bed incineration as well as in processes of the chemical
synthesis of nylon, adipic acid and nitric acid. Due to its inertness, it reaches the
stratosphere undecomposed where, in the long-term, it accumulates to damage
the protecting ozonosphere of the earth. Therefore, for the first time conditions
15 for the global emission reduction of this gas were stipulated at the world
environmental conference in Kyoto in 1997. This requires the application of
suitable catalysts to treat the waste gas streams.

Apart from various noble metals, ceramics, such as modified zeolites and mixed oxides with perovskite structure, can be utilized as feasible catalyst material. Due to their price advantage compared to noble metals and their better temperature resistance, perovskite combinations are considered as being advantageous. In Catal. Lett. (1995), 34 (3, 4) pp. 373-382 N. Gunasekaran describes, among others, catalytic decomposition of laughing gas by mixed oxides with perovskite structure and perovskite-like structure, wherein $\text{La}_{0.8}\text{Sr}_{0.2}\text{MO}_{3-d}$ ($M = \text{Cr, Fe, Mn, Co, Y}$) and $\text{La}_{1.8}\text{Sr}_{0.2}\text{CuO}_{4-d}$ are considered as advantageous catalyst materials.

Due to energy considerations, the particular object of the previous research work predominantly were catalysts which facilitated decomposition of N_2O as completely as possible within a range of 250 °C to 450 °C. Thereby a mixture of an anion defect perovskite of the composition $\text{La}_{1-x}\text{Cu}_x\text{CoO}_{3-d}$, wherein $x = 0 \dots 0.5$, and of a spinel of the composition Co_3O_4 at a 1:1 mass ratio turned out to be particularly advantageous (DE 197 00 490 A1).

However, the catalysts mentioned herein up to now failed at higher temperatures (800°C - 1200°C) as the latter are in particular required for the reduction of the N_2O content in process gases in nitric acid production (900°C).

Due to the stipulations of Kyoto mentioned above there is, particularly for the last mentioned process, an increasing demand for catalysts for the reaction mentioned at the beginning of this specification.

5 The previously known catalysts for the decomposition of N_2O suffer from a nonreversible deactivation at temperatures above $700^\circ C$ owing to sintering processes (noble metal catalysts), to a lack of thermal stability of the skeletal structure (zeolite), or to non-reversible reactions between the transitional metal oxides of the active components with the supporting materials of the kind having a high content of Al_2O_3 .

10 Furthermore, a special feature concerning the application in nitric acid production lies in the required selectivity with respect to other oxides of nitrogen, one of which being, indeed, the objective of the synthesis. Such a selection is not required or even undesired with other processes in the waste gas treatment.

15 Therefore, it is an object of the present invention to provide a catalyst for the selective decomposition of N_2O in a mixture of nitrous gases which is

adapted to be applied in a temperature range of from 700°C to at least 1000°C without any impairment of the catalyst activities.

The object is realized by the present invention.

Summary of the Invention

5 The substitution of conventional Al_2O_3 -containing support materials (for example, alumina or alumino-silicates) by alkaline earth compounds, in particular magnesium oxide, prevents a deactivation of the catalyst by a chemical reaction between the active phase and the support material at temperatures above 700°C as the same takes place in the prior art, for example,
10 by spinel formation between the oxides of the aluminum and of the cobalt. Moreover, different alkaline earth oxides themselves exhibit a certain catalytic activity in dependence on their pore structure when decomposing the laughing-gas.

 The production of the alkaline earth oxide is, for example, carried out by
15 the calcination of a salt, preferably of the carbonate, whereby the calcination temperature depends on the stability of the carbonate of the respective element,

on the desired granularity of the alkaline earth oxide, and on a later application temperature of the catalyst.

5 The oxides and the mixed oxides of the catalytically active component are preferably produced wet chemically by mixed precipitation, drying and thermal decomposition of the dried products. Alternative methods are the production by means of solid-state reaction at high temperatures, pyrolytic processes as well as all other known methods of the powder production.

10 The active components can be added prior or after the calcination of the support material in the form of precursor compounds (salts), oxides or mixed oxides. In addition to the mechanical mixing of both components, there are different methods available for impregnating the support surface with the active component as well as the deposition by precipitation upon the calcined support material with a subsequent fixing by drying and thermal treatment.

15 The mentioned mixtures are plasticized and homogenized under addition of suitable plasticizing aids and water, as known in ceramic manufacturing, in order to produce shaped catalyst elements. It is feasible to add binding agents for increasing the strength, such as silica sol, inorganic polymers in, for

example, the form of magnesium phosphates, aluminum phosphates, and boron phosphates, respectively, or bonding clays, whereby the part of the same has to be kept as low as possible, provided that no alkaline earth compounds are concerned. Said binding agents for increasing the strength can be

5 homogeneously added prior or after the calcination of the alkaline earth salt.

The completion is carried out according to the known ceramic methods, such as granulating or extrusion. By a subsequent release and sintering catalyst elements can be produced in the form of granular material, bulk material, or honeycomb bodies.

10 The effectiveness of the catalysts of the invention is subsequently disclosed by virtue of three embodiments having different proportions of the catalytically active phase. Furthermore, there are added six examples of additions for increasing strength according to the invention.

Brief Description of the Drawings

15 In the drawings:

Fig. 1 is a plot of laughing gas decomposition by a catalyst of the invention with a 0.1 per cent by weight catalytic active phase (active component) as a function of temperature (Example 1);

Fig. 2 is a plot of the selectivity of the catalyst of Fig. 1 towards NO_x ,
also as a function of the temperature;

Fig. 3 is a plot of laughing gas decomposition by a catalyst of the
invention having a 1.5 per cent by weight catalytic active phase
(active component) as a function of the temperature (Example 2);

Fig. 4 is a plot of the selectivity of the catalyst of Fig. 3 towards NO_x
also as a function of the temperature;

Fig. 5 is a plot of laughing gas decomposition by a catalyst of the
invention having a 5.0 per cent by weight catalytic active phase
(active component) as a function of the temperature (Example 3);

Fig. 6 is a plot of the selectivity of the catalyst of Fig. 5 towards NO_x
also as a function of the temperature.

Examples 1-3

A catalyst of the invention in the form of a granular material was tested
by means of a test gas simulating the process gas of the nitric acid production,

said test gas being constituted of 2000 vol.-ppm N_2O ; 9.0 vol.-% NO , 6.0 vol.-% O_2 ; 0.14 vol.-% H_2O ; remainder N_2 . In the case of Examples 1 and 2, the active phase consists of 0.1 weight % and 0.5 weight percent, respectively, of a heavy metal catalyst with the main constituents Mn, Fe, Cr, and Co. In the case of Example 3, the active phase consists 5.0 weight percent of a lanthanum-strontium-manganese-cobalt perovskite. At a space velocity of 10.000 h^{-1} and at a temperature of 800°C , one respective 100% catalytic conversion of the N_2O (Figs. 1, 3, 5) was carried out with each of the catalysts. The NO_x contained in the gas stream is scarcely reduced. It was surprisingly found that a complete conversion of the laughing-gas was virtually obtained independently of the concentration of the active component already at the low content of 0.1 per cent by weight of Example 1 at the 800°C mentioned. A higher content of the active phase, as in Examples 2 and 3, only results in an earlier starting of the reaction without the same being completed at lower temperatures.

Since the alkaline earth compounds, being essential for the invention, are not adapted to form a sufficiently stable ceramic by themselves, it depends on employing such binding agent phases in the course of producing the ceramic catalysts of the invention which exhibit a sufficient strength in the burned state, provided the porous ceramic support material is comprised of at least 95 per

cent by weight of alkaline earth compounds. To this end, there may be added a SiO₂-sol as oxide-sol which contains 5 to 25 weight %, preferably 10 to 15 weight % SiO₂ or there may be added magnesium phosphates, aluminum phosphate and/or boron phosphate as inorganic polymers in a range of from 3 to 20 weight %, preferably 8 to 15 weight % related to the entire mass of the support material, maintaining the condition, however, that the support material is comprised of at least 95 weight % of one or more alkaline earth compounds or there may be added aluminum hydroxide and/or polymeric magnesium silicates as inorganic polymers in a range of from 3 to 20 weight %, preferably 8 to 15 weight % related to the entire mass of the support material, maintaining the condition, however, that the support material is comprised of at least 95 % of one or more alkaline earth compounds.

Example 4

15 percent by weight of a SiO₂-sol with a SiO₂ content of 13% are added to the alkaline earth compounds for the support material. After burning as usual in ceramic technology the SiO₂ part of the ceramic support material exhibiting good strength values amounts to 1.95 per cent by weight.

Example 5

14 percent by weight of a magnesium phosphate containing, among others, 6% MgO and 37% P_2O_5 , are added to the alkaline earth compounds of the support material. After burning, the MgO part of a ceramic support material constituted substantially of CaO amounts to 0.84 per cent by weight and, if the support material substantially consists of MgO, instead, the proportion thereof is increased by the same percentage.

Example 6

12 percent by weight of a magnesium phosphate containing, among others, 8% of Al_2O_3 and 35% P_2O_5 are added to the alkaline earth compounds of the support material. After burning, the Al_2O_3 part of the ceramic support material amounts to 0.96 percent by weight.

Example 7

8 percent by weight of a boron phosphate containing, among others, 36% of B_2O_3 and 57% P_2O_5 are added to the alkaline earth compounds of the support material. After burning, the B_2O_3 part of the ceramic support material amounts to 2.9 percent by weight.

Example 8

5.5 percent by weight of an aluminum oxide precursor consisting of 85% of Al_2O_3 and 15% H_2O are added to the alkaline earth compounds of the support material. After burning, the Al_2O_3 part of the ceramic support material amounts to 4.7 percent by weight.

Example 9

5 percent by weight of a polymeric magnesium silicate, containing, among others, 23.7 percent by weight MgO and 57 percent by weight SiO_2 are added to the alkaline earth compounds of the support material. After burning, the MgO part of a ceramic support material substantially consisting of CaO amounts to 1.2 percent by weight MgO as well as 2.85 per cent by weight SiO_2 and, if the support material substantially consists of MgO , instead, the proportion thereof is increased by the aforementioned percentage of MgO .